## Aspects of Selective Oxidation and Ammoxidation Mechanisms over Bismuth Molybdate Catalysts

II. Allyl Alcohol as a Probe for the Allylic Intermediate<sup>1</sup>

JAMES D. BURRINGTON, CRAIG T. KARTISEK, AND ROBERT K. GRASSELLI

The Standard Oil Company (Ohio), Research Department, 4440 Warrensville Center Road, Warrensville Heights, Ohio 44128

Received June 21, 1979; revised November 14, 1979

The oxidation and ammoxidation of allyl alcohol over MoO<sub>3</sub>, Bi<sub>2</sub>O<sub>3</sub> · nMoO<sub>3</sub> (n = 0, 1, 3), and a multicomponent catalyst ( $M_a^{2+}M_b^{3+}Bi_xMo_yO_z$ ) have been studied as a method of generating  $\sigma$ -allyl complexes analogous to those formed in the selective oxidation of propylene to acrolein. Adsorption experiments and studies using allyl alcohol-1,1- $d_2$  and -3,3- $d_2$  reveal the role of acid/ether-forming sites and oxidation/acrolein-forming sites in the equilibration of C-1 and C-3 of allyl alcohol, and establish hydrogen abstraction as the rate-determining step with  $k_{\rm H}/k_{\rm D} \approx 2.5$  (320°C, oxidation) and 2.1 (430°C, ammoxidation). Relative product distributions for the catalysts studied show the importance of bismuth in the rate enhancement of the hydrogen abstraction step. These results are interpreted in terms of a selective propylene oxidation mechanism in which the initially formed  $\pi$ -complex collapses to an O  $\sigma$ -complex prior to the second hydrogen abstraction to form reduced catalyst and acrolein. In ammoxidation, the analogous N  $\sigma$ -complex undergoes two hydrogen abstractions to produce acrylonitrile.

### INTRODUCTION

The mechanism of selective catalytic oxidation of propylene has been the topic of much study which has recently been reviewed (1). These studies, which include analyses of product distribution, kinetics of oxidation of <sup>2</sup>H- and <sup>13</sup>C-labeled propylenes (2), and the reaction of propylene in the presence of  ${}^{18}O_2$  (3, 4) and  ${}^{18}O$ -labeled catalyst (5), have provided much information concerning the rate-determining step (the formation of an allylic intermediate) and the mechanism of oxygen incorporation (Mars-vanKrevelen mechanism of bulk diffusion) (6) but relatively little concerning the subsequent steps involved in the formation of selective oxidation products. It is generally accepted that  $\alpha$ -hydrogen abstraction from propylene occurs in the rate-determining step. However, the nature of this step and of the allylic intermediate itself is less well understood. EPR evidence has suggested the existence of Mo(V) (7) and allyl radicals (8) as intermediates, while evidence against acrolein (9) and allyl alcohol (4) as intermediates in acrylonitrile and acrolein formation respectively has been presented.

The subsequent steps involved in the conversion of the allylic intermediate to selective products are even less well understood. The isotopic ratios for acrolein and acrylonitrile derived from experiments using deuterium-labeled propylene (2) suggest that the second hydrogen abstraction occurs to form the carbenoid 2 before oxygen insertion, via a  $\pi$ -allyl intermediate (1) which has equal probability of removing a hydrogen atom from either end of the allylic moiety (1) [Eq. (1)]. In the case of ammoxidation, the carbene-like intermediate undergoes a third hydrogen abstraction from the methylene end and nitrogen insertion to form acrylonitrile [Eq. (1)].

<sup>&</sup>lt;sup>1</sup> Presented at the Gordon Research Conference, Symposium on Catalysis, New London, New Hampshire, June 29, 1979.



Based on relative stabilities of allyl radicals vs carbene it is probable that sequential removal of hydrogens would require more energy for the removal of the second hydrogen (and the third for acrylonitrile formation), an assumption that is consistent with quantum chemical calculations (9). However, this conclusion is contrary to experimental evidence, which supports the removal of the first hydrogen to form an allylic intermediate as the rate-determining step.

An alternate mechanism is one in which the oxygen insertion occurs prior to the second  $\alpha$ -hydrogen abstraction to form a  $\sigma$ allyl molybdate 3 either via a  $\pi$ -allyl molybdate 1a or directly from propylene [Eq. (2)]. The step in which 3 is converted to acrolein,



which involves a second  $\alpha$ -hydrogen abstraction, is now facilitated by the presence of the C-O bond. Intermediates similar to **3** have been previously proposed (10).

Since either end of the allylic fragment in la has equal probability of collapsing on an oxygen, the same isotopic product distribution, based on the known isotope effect, is expected as for the sequential hydrogen removal mechanism, when one starts with propylene deuterated in the 1 or 3 position, provided that la and 3 are in rapid equilibrium with respect to hydrogen abstraction from 3 to form acrolein. This same reasoning applies for ammoxidation by simply replacing the Mo=O moiety with Mo=NH followed by two hydrogen abstractions.

The intermediate 3 may be considered a molybdenum(V) ester. The analogous Mo(VI) ester(4), which should be accessible via condensation of allyl alcohol with  $MoO_3$ , contains the Mo=O necessary to effect hydrogen abstraction and should thus be a good model for 3 [Eq. (3)]. The importance of metal-oxygen double bonds in catalytic oxidation has been discussed (11).

A structure similar to 4 has been observed spectroscopically as a surface inter-

$$\begin{array}{c} & & & & \\ & & & \\ + & & & \\ & & & & \\ & & & \\ & & & \\ & & & \\ & & & & \\ & & & \\ & & & &$$

mediate in the selective oxidation of propylene with Mo-containing catalysts (12a). The formation of esters of molybdic acid has been proposed in the reaction of alcohols with silica-fixed MoO<sub>3</sub> (12b). Likewise, the analogous esters 5 and 6 formed from the reaction of allyl alcohol with  $Bi_2O_3 \cdot MoO_3$  and  $Bi_2O_3 \cdot 3MoO_3$  ( $\gamma$ and  $\alpha$ -bismuth molybdate, respectively) may also be studied [Eqs. (4) and (5)].



A study of the relative reactivity and product distribution resulting from reaction of these  $\sigma$ -allyl molybdates will provide a theoretical basis for the differences observed in the oxidation and ammoxidation over the various bismuth molybdates and the function of the atomic components of each.

In this work, we have studied in detail the reaction of allyl alcohol with molybdenum trioxide, bismuth(III) oxide,  $\alpha$ - and  $\gamma$ bismuth molybdate, and a multicomponent system. Evidence for the formation of  $\sigma$ allyl molybdates 4, 5, and 6 and conclusions concerning their mechanisms of reaction and relation to the selective oxidation and ammoxidation of propylene will be presented. These conclusions are based on product distributions, adsorption studies, and a study of the reactions of <sup>18</sup>O-allyl alcohol and allyl alcohol-1,1- $d_2$  and -3,3- $d_2$ with these catalysts.

It should be noted at the outset that it is not our contention that desorbed allyl alcohol is an intermediate in the catalytic oxidation of propylene (4). Its use in this study is only as a probe for the *in situ* generation of  $\sigma$ -complexes analogous to those formed in propylene oxidation, for the purpose of gaining mechanistic information concerning those steps after the rate-determining allylic hydrogen abstraction.

### **EXPERIMENTAL**

## General

All experiments were performed by the pulse method using the microreactor gas chromatograph system described previously (13). Proton nuclear magnetic resonance spectra (NMR) were recorded on a Varian EM 390 (90 MHz) interfaced with a Nicolet 1180 computer. Signals are reported in parts per million downfield from tetramethylsilane with the following notations: s, singlet; d, doublet; t, triplet; q, quartet; m, multiplet, br, broad.

Mass spectra were recorded using a Finnigan 4000 glc/ms system equipped with a Carbowax 20M 100-ft SCOT (support coated open tube) capillary column. Ionizing voltage and column temperature were 10.7 eV, 50°C and 13.7 eV, 80°C for acrolein and acrylonitrile, respectively. Infrared spectra were recorded on a Nicolet 7199 Fourier Transformer instrument.

partition Gas-liquid chromatography (glc) analyses and separations employed a Varian 3760 (flame ionization or thermal conductivity, helium) using either a Houdry system described previously for pulse reactor work (13) or a 6-ft  $\times$  1/8-in. stainlesssteel column packed with 5% Carbowax 20 M on Anakom SD 80/100 mesh, with a flow rate of 30 cm<sup>3</sup> min<sup>-1</sup> at 90°C column temperature, for analysis of the prepared labeled compounds. Unlabeled allyl alcohol (MCB, 98+%) was used without further purification.

Preparation of unsupported fixed-bed (20-35 mesh) MoO<sub>3</sub>, Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub> and Bi<sub>2</sub>O<sub>3</sub> · MoO<sub>3</sub>, Bi<sub>2</sub>O<sub>3</sub> (13), and  $M_a^{2+}M_b^{3+}$  Bi<sub>x</sub>Mo<sub>y</sub>O<sub>z</sub> (14) has been described.

Relevant catalyst properties are shown in Table 1. Catalysts used in all experiments were 100% active phase.

Allyl alcohol-3,3- $d_2$  was prepared by the method of McMichael (15) in two steps from propargyl alcohol. Repeated equilibration of propargyl alcohol with D<sub>2</sub>O (SIC, 99.8 atom% D) containing BaO resulted in 88.7 and 92.2% deuterium exchange at the acetylenic (t, 2.39 $\delta$ ) and hydroxyl position (brs, 3.00 $\delta$ ) respectively by NMR (CDCl<sub>3</sub>) integration compared to methylene group (s, 4.13 $\delta$ ). Reduction of this mixture with LiAlH<sub>4</sub> in ether with D<sub>2</sub>O workup gave, after microspinning band distillation, a mix-

TABLE 1

Catalyst	Properties
----------	------------

Catalyst	Density (g/cm <sup>3</sup> )	S.A. (m <sup>2</sup> /g)	Rel. acidity <sup>a</sup>
 MoO <sub>3</sub>	1.8	0.7	3.0
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	0.79	1.7	2.3
Bi <sub>2</sub> O <sub>3</sub> · MoO <sub>3</sub>	1.0	2.2	1.2
Bi <sub>2</sub> O <sub>3</sub>	4.4	0.2	0.1
$M_a^{2+}M_b^{3+}Bi_xMo_yO_z$		4.7	2.9

<sup>a</sup>  $\mu$ mole of NH<sub>3</sub> irreversibly adsorbed when a 0.9cm<sup>3</sup> pulse of 19% NH<sub>3</sub>, 81% He (7  $\mu$ mole NH<sub>3</sub>) is passed over 3.92 m<sup>2</sup> of catalyst at 200°C, 3-sec contact time. ture of allyl alcohols [>96% pure (by glc), 10% yield from propargyl alcohol]:  $3,3-d_2$ (77.3%),  $2,3-d_2$  (8.9%), 3-d (13.4%), 2-d(0.1%)  $d_0$  (0.4%), 86.4% OH, by NMR (CDCl<sub>3</sub>) from relative integration of the vinyl methylene (m, 4.97–5.23 $\delta$ ), methine (m, 5.77–5.97 $\delta$ ), methylene (d of d, 4.03 $\delta$ ), and OH (t, 2.20 $\delta$ ) proton signals. This mixture will be referred to as allyl alcohol (77%  $3,3-d_2$ ).

Conversion to the trimethylsilyl ether was accomplished by warming a mixture of 20  $\mu$ l pyridine, 10  $\mu$ l of the allyl alcohol  $(77\% 3,3-d_2)$  from above, and 1 µ1 bistrimethylsilyltrifluoroacetamide (BTSTA, Regisil, Regis Chemical Co.) at 80°C for 1 hr in a stoppered tube. The mass spectrum of the glc peak corresponding to allyl trimethylsilyl ether gave a  $d_2: d_1: d_0$  ratio (as peaks, measured by the M-15 117:116:115) of 86.5:13.5:0. (ratio from NMR = 86.2 : 13.5 : 0.4.)

Allyl alcohol-1, 1- $d_2$  was prepared by the method of Schuetz and Millard (16) by the reduction of acrylyl chloride (Aldrich, 98%) with lithium aluminum deuteride (ICN) in 22% isolated yield after microspinning band distillation [>97% pure by glc (Flame Ionization Dectector)]; NMR (CDCl<sub>3</sub>) showed >98% 1,1- $d_2$ , and ~21 mole% water, confirmed by glc using a thermal conductivity detector. This alcohol was converted to the trimethylsilyl ether and analyzed by mass spectroscopy as before to give a  $d_2: d_1: d_0$  ratio of 98.2:1.8:0.

Allyl alcohol-1,1- $d_2$  and -3,3- $d_2$  (55:45 mixture of allyl alcohol-1,1- $d_2$ :3,3- $d_2$ ) was prepared by isomerization (300°C, 25 min) of the allyl trifluroacetate resulting from the reaction of allyl alcohol-1,1- $d_2$  and trifluroacetic anhydride with subsequent hydrolysis at 110°C.

<sup>18</sup>O-Allyl alcohol was prepared by a modification of the method of Murty and Curl (17). To a mixture of acrolein dimethyl acetal (8.1 g, 79.4 mmole) and  $H_2^{18}O$  (2.0 g, 100 mmole, Prochem/Isotopes, 99.0 atom% <sup>18</sup>O) was added one drop of concentrated sulfuric acid cautiously and the re-

sulting pale-yellow solution distilled. The fraction boiling at 50-56°C was collected in 10 ml dry ether at 0°C to which had been added a few crystals of hydroquinone. To a stirred suspension of lithium aluminum hydride (1.0 g, 28.5 mmole) in 30 ml dry ether, cooled in an ice-salt bath, was added the above ether solution of <sup>18</sup>O-acrolein over 1 hr under an argon atmosphere. The temperature was maintained between 5 and 10°C during the addition. After completion of the addition, the reaction mixture was stirred at 0°C for 30 min, the ice bath removed, and 3 ml of a 15% NaOH solution added slowly. The mixture was allowed to stir for 10 min, at which time a white granular precipitate formed. The mixture was then filtered, the precipitate washed with ether  $(5 \times 10 \text{ ml})$ , the resulting ether extract dried  $(Na_2SO_4)$ , filtered, concentrated to  $\sim 6$  ml on a rotary evaporator, and the resulting solution distilled on a 24-cm microspinning band column. The fraction boiling at 89-90°C (1.03 g, 22% from acrolein dimethyl acetal) contained >97% allyl alcohol by glc; NMR and ir were also consistent with allyl alcohol; mass spectrum (70 eV) showed <sup>18</sup>O: <sup>16</sup>O ratio (m/e 60: 58) of 96.3: 3.7.

Attempted synthesis by the reaction of allyl iodide with  $H_2O$  in the presence of silver nitrate gave allyl nitrate as the major product.

Oxidation of unlabeled allyl alcohol is shown in Figs. 1 and 2. The effect of gaseous oxygen in allyl alcohol oxidation and relative product distributions from npropanol and allyl alcohol oxidations are shown in Table 2 and 3, respectively.

Allyl alcohol ammoxidation and allyl amine oxidation are shown in Figs. 5 and 6, respectively.

Effect of diluent on product distribution for the reaction of allyl alcohol with  $MoO_3$ and  $Bi_2O_3 \cdot MoO_3$  is shown in Table 6.

Adsorption studies for allyl alcohol and pyridine were performed by following the amount of adsorption vs gas-phase mole fraction when samples of alcohol or pyridine in *n*-octane were pulsed over  $MoO_3$  (0.5 cm<sup>3</sup>, 0.98 g, 0.7 m<sup>2</sup>) at 135°C, 1-sec contact time, using a constant gas-phase pulse size. Adsorption of allyl alcohol in pyridine was performed by this same method, substituting pyridine for *n*-octane in the above adsorption experiments. Further experimental details and the results of these experiments are given in Fig. 3.

### Isotopic Experiments

Allyl alcohol (98% 1,1- $d_2$  or 77% 3,3- $d_2$ ) neat, or in octane, pyridine, or 2-methoxy pyridine for oxidation (320°C) or 3 *M* in 28% ammonium hydroxide solution for ammoxidation (430°C), was injected over MoO<sub>3</sub> and Bi<sub>2</sub>O · 3MoO<sub>3</sub> and the peaks corresponding to acrolein or acrylonitrile, and allyl alcohol were collected in dry-icecooled capillary tubes for NMR or mass spectral analysis. Experimental details and results are shown in Tables 5, 7, 8, and 9. A control experiment using a reactor filled with fused quartz showed that no thermal isomerization of allyl alcohol-1,1- $d_2$ , or that resulting from glc analysis, was occurring.

Reaction of <sup>18</sup>O-allyl alcohol and Mo<sup>16</sup>O<sub>3</sub> at 320°C was studied as a function of pulse time (Fig. 4) and diluent (Table 10).

Relative rates of reaction of unlabeled and allyl alcohol (98%  $1,1-d_2$ ) over MoO<sub>3</sub> and Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub> were determined at 320°C, at a constant surface area (0.7 m<sup>2</sup>) and 0.25-sec contact time by consecutive injections of each under the same reaction conditions. Results are shown in Table 4.

### RESULTS

## 1. Yields vs Allyl Alcohol Concentration for $MoO_3$ and $Bi_2O_3 \cdot 3MoO_3$

(a)  $MoO_3$  (Fig. 1). As is known from literature studies (4) the oxidation of allyl alcohol over  $MoO_3$  gives acrolein in high yield. In this work, the reaction of allyl alcohol in aqueous solution with  $MoO_3$  at  $320^{\circ}$ C as a function of mole percent in the gas phase shows a very high conversion to acrolein (95%) at low allyl alcohol concentration. Upon increasing the alcohol con-



FIG. 1. Yields vs allyl alcohol mole percent for reaction with MoO<sub>3</sub> at 320°C. 0.98 g ( $0.5 \text{ cm}^3$ ,  $0.7 \text{ m}^2$ ) MoO<sub>3</sub>, 0.25 sec. Catalyst oxidized under air stream at 450°C for 30 min between runs. Pulse size =  $1.7 \text{ cm}^3$  ( $35 \mu$ mole allyl alcohol + water).

centration, the yield of acrolein drops due to lower conversion of alcohol and formation of diallyl ether, a dehydration product, and propylene and 1,5-hexadiene which are the  $2e^-$  and  $1e^-$  reduction products, respectively, of allyl alcohol. This suggests that the formation of propylene and 1,5-hexadiene reflects a  $2e^-$  and  $1e^-$  reoxidation of surface reduced sites. While the yields of diene and ether increase with increasing alcohol mole percent, the 1,5-hexadiene yield increases much faster at higher concentrations, suggesting a higher order in allyl alcohol for the rate of formation of diene than for that of ether.

(b)  $Bi_2O_3 \cdot 3MoO_3$  (Fig. 2). As for the MoO<sub>3</sub>, a high conversion to acrolein occurs at low allyl alcohol concentrations. However, the yield of propylene is much greater than for MoO<sub>3</sub>. This reflects the greater ease of reoxidation of reduced sites for  $\alpha$ -bismuth molybdate than for MoO<sub>3</sub> (18). The increase in propylene yield with mole percent alcohol injected suggests a higher order dependence on alcohol concentration than for acrolein formation. The dependence of acrolein and diene yield on concentration is similar to that for MoO<sub>3</sub> but

less diene is formed since many more of the reduced sites are reoxidized via propylene formation. The low ether yield when compared to  $MoO_3$  reflects the lower surface acidity of  $\alpha$ -bismuth molybdate in effecting this dehydration reaction.

The addition of gaseous oxygen to the pulse results in a large increase in acrolein selectivity mainly due to decrease in propylene yield (Table 2). This is probably due to reaction of active surface oxygen rather than lattice oxygen, as has been seen by other workers at this temperature  $(320^{\circ}C)$  (4).

The rate of formation of propionaldehyde from n-propanol is about five times slower than that of acrolein from allyl alcohol (Table 3). Thus, the double bond enhances but is not necessary for oxydehydrogenation.

## 2. Relative Rates of Reaction of Allyl Alcohol- $d_0$ and -1, $1-d_2$ over $MoO_3$ and $Bi_2O_3 \cdot 3MoO_3$

In order to ascertain the nature of the rate-determining step in this reaction, we have measured the relative rate of oxida-



FIG. 2. Yields vs allyl alcohol mole percent for reaction with  $Bi_2O_3 \cdot 3MoO_3$  at 320°C. 0.4 g (0.5 cm<sup>3</sup>, 0.7 m<sup>2</sup>)  $Bi_2O_3 \cdot 3MoO_3$ , 0.25 sec. Catalyst reoxidized under air at 450°C, 30 min between runs. Pulse size = 1.7 cm<sup>3</sup> (35  $\mu$ mole allyl alcohol + water).

### TABLE 2

Comparison of Reactions of Allyl Alcohol with  $Bi_2O_3 \cdot 3MoO_3$  in the Presence and Absence of  $O_2$ ,  $320^{\circ}C^{\alpha}$ 

Conditions	Percentage	Percentage yields (normalized)									
	of AA	$\overline{CO_2}$	C <sub>3</sub> =	Acrolein	HD	PhH	AE	C bal.			
Without O <sub>2</sub> <sup>b</sup>	91.87	0.04	28.78	55.66	5.79	0.63	0.97	103.8			
With O <sub>2</sub> <sup>c</sup>	94.97	2.70	3.92	86.82	0.89	—	0.64	103.3			

<sup>a</sup> 0.5 cm<sup>3</sup> (0.4 g, 0.7 m<sup>2</sup>)  $Bi_2O_3 \cdot 3MoO_3$ , 0.25-sec contact time; AA = allyl alcohol, HD = 1,5-hexadiene, AE = diallyl ether, PhH = benzene.

<sup>b</sup> 12.1  $\mu$ mole allyl alcohol per pulse (0.9  $\mu$ l of 13.4 Maq).

<sup>c</sup> 12.1  $\mu$ mole allyl alcohol + 36.9  $\mu$ mole O<sub>2</sub>.

tion of allyl alcohol-1,1- $d_2$  and unlabeled allyl alcohol.

The results (Table 4) indicate a faster rate of both overall reaction and acrolein formation for allyl alcohol- $d_0$  than for allyl alcohol-1,1- $d_2$  ( $kd_0/kd_2 = 1.2$ ). This result reflects a dilution of the true isotope effect [ $k_H/k_D$  (max, 320°C) = 2.5] by formation of products which involve no C-H (D) bond breaking (ether, diene, propylene). This low  $kd_0/kd_2$  also results, in part, from equilibration of the two terminal carbons of allyl alcohol 1,1- $d_2$  to form allyl alcohol-3,3- $d_2$ along with oxidation to both acrolein-1-dand acrolein-3,3- $d_2$  as discussed below in the section on oxidation of allyl alcohol-1-1 $d_2$  and -3,3- $d_2$ .

This indicates that the rate-determining step in the selective oxidation of allyl alcohol is allylic hydrogen abstraction to form acrolein which corresponds to the fast second hydrogen abstraction in propylene oxidation. Thus, information concerning the role of the elemental components of the catalyst in this second hydrogen abstraction step can be obtained by a comparison of the reactions of allyl alcohol with catalysts of varying composition, discussed in the next section.

## 3. Comparison of $MoO_3$ and $Bi_2O_3 \cdot nMoO_3$ (n = 3, 1, 0)

Table 5 shows the relative product yields in the reaction of allyl alcohol with the five catalysts studied, namely, MoO<sub>3</sub>,  $\alpha$ - and  $\gamma$ bismuth molybdate, Bi<sub>2</sub>O<sub>3</sub>, and a multicomponent (MC) system at 320°C. The order of decreasing activity and decreasing conversion to acrolein in this series follows the order MC >  $\gamma > \alpha > MoO_3 > Bi_2O_3$ . In the MoO<sub>3</sub>/bismuth molybdate series, the successive introduction of bismuth into the molybdate esters formed facilitates the abstraction of hydrogen in the rate-determining step to form acrolein.

Bismuth oxide, however, is very inactive because it lacks the chemisorption site for

Starting alcohol	Percentage		Perce	ntage yields	(normalized)	
alconor	of alcohol	C <sub>3</sub> =	Aldehyde (k)	Ether	1,5-Hexadiene	Benzene
n-Propanol	20.1	10.6	7.6 (1.0)	2.0		
Allyl alcohol	72.0	3.1	33.9 (5.2)	14.0	18.7	2.3

TABLE 3

Comparison of Reactions of Allyl Alcohol<sup>a</sup> and n-Propanol<sup>a</sup> over MoO<sub>3</sub> (320°C)<sup>b</sup>

<sup>a</sup> 10.4 µmole per pulse, injected neat.

<sup>b</sup> 0.5 sec (0.98 g, 0.7 m<sup>2</sup>), 0.25-sec contact time.

### TABLE 4

Product Distributions for Reaction of Allyl Alcohol- $d_0$  and  $-1, 1-d_2$  over MoO<sub>3</sub> and Bi<sub>3</sub>O<sub>3</sub> · 3MoO<sub>3</sub> at 320°C, 0.25 sec, 0.7 m<sup>2a</sup>

Catalyst	Allyl alcohol	AA	Acrolein	C3=	HD	PhH	AE	Selectivity to acrolein	$kd_0/kd_2$
MoO <sub>3</sub>	$d_0$	53.9	28.7	0.6	7.8	0.7	8.4	62.2	1.22
-	$1, 1 - d_2^{b}$	60.2	21.9	0.5	6.6	0.8	10.1	55.0	
$Bi_2O_3 \cdot 3MoO_3$	$d_0^c$	31.1	41.2	16.8	7.6	2.1	1.1	59.8	1.19
	$1, 1 - d_2^{d}$	37.6	35.7	15.6	7.4	2.3	1.5	57.2	

<sup>a</sup> 1.3  $\mu$ l of 13.4 *M* injected per pulse, AA = allyl alcohol, HD = 1,5-hexadiene, AE = diallyl ether, PhH = benzene.

<sup>b</sup> Average of 4 runs.

<sup>c</sup> Average of 2 runs.

<sup>d</sup> Average of 3 runs.

the allyl molbydate formation, while in the multicomponent system, both bismuth and other di- and trivalent metals facilitate this hydrogen abstraction.

Thus, since the molybdate ester is formed in a fast step, these results show that bismuth is the critical element in facilitating the hydrogen abstraction from the molybdate intermediate, as long as enough Mo is present to allow fast formation of the allyl molybdate.

The analagous results for propylene oxidation (13) show that the relative rates for simple bismuth molybdates are in decreasing order,  $\beta \approx \alpha > \gamma > MoO_3 \sim Bi_2O_3$ . This is consistent with a rate-determining step which requires activation of propylene by both chemisorption on Mo centers and hydrogen abstraction on Bi centers. The  $\gamma$ - phase and  $Bi_2O_3$  have too few chemisorption sites while MoO<sub>3</sub> has no  $\alpha$ -hydrogen abstracting sites, and thus these catalysts are less active. The  $\alpha$ - and  $\beta$ -phases are the most active and selective catalysts of the simple Bi/Mo series since they have a favorable balance of the two sites necessary to effect the rate-determining first hydrogen abstraction.

The formation of ether and propylene, as stated earlier, reflects the catalyst's acidity and its ease of reduction, respectively. Thus, the multicomponent system is both the easiest to be reduced and to be reoxidized by allyl alcohol, while  $MoO_3$  has the highest and  $Bi_2O_3$  the lowest surface acidity. (See Table 1.)

The yield of products does not change drastically with pulse number for any of the

Catalyst	cm <sup>3</sup> catalyst	Percentage yields (normalized) <sup>b</sup>						Acrolein (%) <sup>c</sup>		AA (%) <sup>c</sup>		
		$CO_2$	C <sub>3</sub> =	Acrolein	AA	HD	PhH	AE	$1 - d_1$	3,3- <i>d</i> <sub>2</sub>	$1, 1-d_2$	3,3-d <sub>2</sub>
MoO <sub>3</sub>	0.5	Trace	2.0	13.3	64.0	4.1	0.7	15.9	40.6	59.3	58.9	41.1
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	0.5	Trace	17.4	29.5	42.3	7.2	2.0	1.4	47.1	52.9	77.0	23.0
Bi <sub>2</sub> O <sub>3</sub> · MoO <sub>3</sub>	0.32	Trace	21.5	38.9	33.2	4.7	0.9	0.9	44.1	55.9	74.0	26.0
Bi <sub>2</sub> O <sub>3</sub>	0.8	0.2	1.7	13.2	80.4	3.8	_	0.7	82.1	17.9	90.9	9.1
$M_a^{2+}M_b^{3+}Bi_xMo_yO_x$	0.17	—	21.5	49.8	19.3	4.0	0.8	4.5	35.1	64.9	58.3	41.7

TABLE 5

Product and Isotopic Dist	ribution from Allyl	Alcohol-1,1-d2 Ox	idation (Low Conversion) <sup>a</sup>
---------------------------	---------------------	-------------------	---------------------------------------

<sup>a</sup> 0.25-sec contact time, 0.7 m<sup>2</sup> total surface area, 42 µmole (3 µl neat allyl alcohol) injected, 320°C.

<sup>b</sup> AA = allyl alcohol, HD = 1,5-hexadiene, AE = diallyl ether, PhH = benzene.

" Ratios by NMR.

243

catalysts, despite the fact that  $MoO_3$  makes very little propylene, whereas  $Bi_2O_3 \\\cdot \\3MoO_3$  and  $Bi_2O_3 \\\cdot \\MoO_3$  make a considerable amount. Thus, the bulk diffusion of lattice oxygen to reduced sites must be fast enough in all of these catalysts to keep up with each two-electron oxidation of allyl alcohol to acrolein and benzene. Since the relative rates of reoxidation by  $O_2$  (lattice mobility) decrease in the order  $Bi_2O_3 \\\cdot \\MoO_3 > Bi_2O_3 \\\cdot \\3MoO_3 > MoO_3 (18)$ , the rapid reconstruction of reduced catalytic sites is much faster than the rate-determining step (hydrogen abstraction) in these reactions.

### 4. Effect of Diluent

The effect of diluent on product distribution for the reaction of allyl alcohol with  $MoO_3$  and  $\alpha$ -bismuth molybdate at 320°C reveals some important features of the mechanism of this reaction (Table 6). For both these catalysts, a comparison of the reaction using water or pyridine bases with that using an inert diluent, *n*-octane, was obtained.

For  $MoO_3$ , the reaction using water as diluent gives slightly less acrolein yield, but much less converison due to a smaller yield of reduced products, propylene and 1,5hexadiene. When the diluent is pyridine or 2-methoxypyridine, the ether and propylene yields are reduced to nearly zero, while the acrolein yield remains unchanged. For  $\alpha$ -bismuth molybdate, the same general trends are seen, except that ether yields are very low regardless of solvent, due to its lower surface acidity compared to MoO<sub>3</sub>.

Several important mechanistic conclusions follow from these results. First, since acrolein yield is insensitive to base, acid sites are not involved in the formation of acrolein. However, the dehydration of allyl alcohol to form diallyl ether is occurring on acid sites, since its formation is drastically reduced on addition of base. In addition, propylene is probably formed from reduced acid sites, a process which is inhibited by pyridine.

These results suggest that two types of sites are involved in the reaction of allyl alcohol with  $MoO_3$  and bismuth molybdate, namely, acid sites, which are involved in ether formation, and oxidizing sites, on which acrolein is formed. In order to gain more information concerning the relative number of these sites, low-temperature adsorption studies were performed, discussed in the following section.

### 5. Adsorption Experiments

Adsorption studies were performed at

	Diluent <sup>d</sup>			Percentage				
		$C_3^{=}$	Acrolein	AA	HD	PhH	AE	selectivity
(1) <b>MoO</b> <sub>3</sub> <sup><i>b</i></sup>	n-Octane	6.4	66.0	3.8	15.4	1.4	7.0	68.6
	$H_2O$	0.8	61.7	24.1	3.5	0.8	9.0	81.3
	Pyr	0.1	67.6	20.7	10.8	0.5		85.2
	2-MPyr	1.5	63.2	22.7	12.1	TR	0.3	85.2
(2) $\operatorname{Bi}_2\operatorname{O}_3 \cdot 3\operatorname{MoO}_3^c$	n-Octane	27.1	63.0	0.7	5.0	3.8	0.4	63.4
	$H_2O$	21.8	60.9	11.3	3.6	2.2	0.3	68.7
	Pyr	20.3	64.2	10.3	4.8	0.4		71.6

TABLE 6

Diluent Effect on Product Distribution from Allyl Alcohol +  $MoO_3$  and  $Bi_2O_3 \cdot 3MoO_3$ ,  $320^{\circ}C^{\alpha}$ 

<sup>*a*</sup> All experiments: vapor phase feed = 5.8  $\mu$ mole allyl alcohol, 15.1  $\mu$ mole diluent; 0.7 m<sup>2</sup> catalyst; 0.25-sec contact time; AA = allyl alcohol, HD = 1,5-hexadiene, AE = diallyl ether, PhH = benzene.

<sup>b</sup> 0.5 cm<sup>3</sup> (0.98 g) MoO<sub>3</sub>.

 $^{\rm c}$  0.5 cm  $^3$  (0.4 g)  $Bi_2O_3\cdot 3MoO_3.$ 

<sup>d</sup> Pyr = pyridine; 2-MPyr = 2-methoxy pyridine.

135°C by increasing the mole fraction of allyl alcohol in *n*-octane and measuring the amount of alcohol in the effluent, using the apparatus described previously. pulse These experiments (squares, Fig. 3) gave a site density of about  $2.0 \times 10^{18}$  sites/m<sup>2</sup>. The corresponding experiments for pyridine adsorption (triangles) gave an acid site density of  $1.5 \times 10^{18}$  sites/m<sup>2</sup>. A series of experiments were then performed in which the alcohol adsorption was measured as a function of gas-phase mole percent of alcohol in pyridine. This curve (circles) shows an inflection point corresponding to  $0.7 \times$  $10^{18}$  molecules/m<sup>2</sup>.

These results are consistent with a dualsite structure for  $MoO_3$  in which the total number of alcohol chemisorption sites  $(2 \times 10^{18}/m^2)$  is composed of acroleinforming sites  $(7 \times 10^{17}/m^2)$  on which allyl alcohol is chemisorbed exclusively in the presence of excess pyridine, represented by the portion of the curve (Fig. 3) to the left of inflection, and about twice as many acid sites  $(1.5 \times 10^{18}/m^2)$  on which allyl alcohol is chemisorbed in the region of lower pyridine concentration, to the right of inflection.

## 6. Oxidation and Ammoxidation of Allyl Alcohol-1,1-d<sub>2</sub> and -3,3-d<sub>2</sub>

In this study, we are mainly concerned with the reaction of allyl alcohol on acrolein-forming sites to form the allyl molybdate intermediate. Thus, our experiments using deuterated allyl alcohols, which will determine the feasibility of our proposed allyl molybdate intermediate (analogous to 4), must be interpreted in terms of the reaction which occurs on acrolein-forming sites.

(a) Reactions in the absence of base. The reactions observed here are a composite of those occurring on acid and acroleinforming sites.

The acrolein  $d_1/d_2$  ratio observed from oxidation of allyl alcohol-1,1- $d_2$  or -3,3- $d_2$ under high conversion conditions (~3 cm<sup>3</sup>



FIG. 3. Adsorption of allyl alcohol and pyridine on MoO<sub>3</sub> at 135°C. 0.9 g (0.5 cm<sup>3</sup>, 0.7 m<sup>2</sup>) MoO<sub>3</sub> used. Pulse size = 0.35 cm<sup>3</sup> (10.4  $\mu$ mole total).

Oxidation (320°C)	Starting alcohol	Products	Experimental %"	Theoretical % (Allylic intermediate) <sup>f</sup>	Percentage conversion
	CH <sub>2</sub> CHCD <sub>2</sub> OH <sup>a</sup>	Acrolein- $d_2$	69.4 <sup>g</sup>	70.1	72.5
		$-d_1$	30.6 <sup>g</sup>	29.7	
		$-d_0$	0.0	0.2	
	CD <sub>2</sub> CHCH <sub>2</sub> OH <sup>b</sup>	Acrolein- $d_2$	62.1	61.4	75.3
		$-d_1$	33.3	35.6	
		$-d_0$	4.6	2.2	
Ammoxidation (430°C)					
	CH <sub>2</sub> CHCD <sub>2</sub> OH <sup>c</sup>	Acrylonitrile-d <sub>2</sub>	68.6	67.4	93.3
		$-d_1$	1.6	1.6	
		$-d_0$	29.8	31.0	
	$CD_2CHCH_2OH^d$	Acrylonitrile-d2	61.5	58.1	91.6
		$-d_1$	12.3	11.6	
		$-d_0$	26.2	30.4	

# Isotopic Distribution for Products in Oxidation and Ammoxidation of Allyl Alcohol over MoO<sub>3</sub> (2.9 cm<sup>3</sup>), 2 sec (High Conversion)

TABLE 7

<sup>*a*</sup> 2  $\mu$ l of 11.8 *M* alcohol in H<sub>2</sub>O per pulse; average of 8 runs.

<sup>b</sup> 2  $\mu$ l of 14.7 M alcohol in H<sub>2</sub>O per pulse; average of 9 runs.

<sup>c</sup> 3.3 μl of 2.7 M alcohol, 10.9 M NH<sub>3</sub> in H<sub>2</sub>O; average of 6 runs.

<sup>*d*</sup> 2  $\mu$ l of 3 *M* alcohol, 12 *M* NH<sub>3</sub> in H<sub>2</sub>O; 13.7 eV (AN). Similar runs in H<sub>2</sub>O or using 11  $\mu$ mole of neat allyl alcohol + 37  $\mu$ mole of anhydrous NH<sub>3</sub> gave similar results.

<sup>e</sup> By mass spectroscopy at 10.7 eV (acrolein), 13.7 eV (AN).

<sup>f</sup> Calculated  $k_{\rm H}/k_{\rm D}$  (320°C) = 2.5; (430°C) = 2.2.

<sup>g</sup> Analysis by NMR gave a 65.9:34.1:0 ratio.

catalyst, 2-sec contact time) indicates that  $alcohol occurs for MoO_3$  in both oxidation total equilibration of C-1 and C-3 of allyl and ammoxidation reactions (Table 7) and

### TABLE 8

Isotopic Distribution for Products in Oxidation of Allyl Alcohol over Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub> (3.0 cm<sup>3</sup>) at 320°C, 2 sec (High Conversion)

Starting alcohol	Products	Experimental %"	Theoretical %					
			Allyl	100% retention	% conv.			
CH <sub>2</sub> CHCD <sub>2</sub> OH <sup>b</sup>	Acrolein- $d_2$	54.1	70.1	0	97.9			
	$-d_1$	44.3	29.7	99.5				
	$-d_0$	1.6	0.2	0.5				
	Propylene- $d_2$	96.7 (91.0)	100	100				
	(32.3% conversi	ion)						
	$-d_1$	2.1 ( 3.0)	0	0				
	$-d_0$	1.2 (0.4)	0	0				
	$-d_3$	0 (5.6)	0	0				
CD <sub>2</sub> CHCH <sub>2</sub> OH <sup>c</sup>	Acrolein- $d_2$	69.4	61.4	84.5	99.1			
	$-d_1$	30.6	35.6	14.8				
	$-d_0$	0	2.2	0.5				

<sup>a</sup> By mass spectroscopy at 10.7 eV; numbers in parentheses are for catalyst after 5 pulses.

<sup>b</sup> 2.1  $\mu$ l of 11.8 M alcohol per pulse; average of 5 pulses.

<sup>c</sup> 2.0 µl of 14.7 M alcohol per pulse; average of 5 pulses.

### **TABLE 9**

Effect of Base on Product and Isotopic Distribution for Reaction of Allyl Alcohol- $d_2$ and Propylene- $d_2$  at  $320^{\circ}C^a$ 

Catalyst	Catalyst Diluent <sup>e</sup> AA			Percentage yields <sup>6</sup>							Acrolein (%)"		AA (%) <sup>4</sup>	
	AA: solvent	C3-	Acrolein	AA	HD	PhH	AE	1- <i>d</i> 1	3,3-d <sub>2</sub>	1,1-d <sub>2</sub>	3,3-d			
 MoO3	n-Octane	1,1-d <sub>2</sub>	1.7	4.4	30.1	38.2	7.1	1.5	19.0	41.8	58.2	56.7	43.3	
MoO <sub>3</sub>	2-MPyr	$1, 1 - d_2$	1.7	0.6	27.4	64.5	6.9	0.0	0.8	56.0	44.0	72.2	27.8	
MoO <sub>3</sub>	Pyr	$1, 1 - d_2$	0.4	0.0	48.8	46.5	4.7	0.0	е	57.0	43.0	77.3	22.7	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	n-Octane	$1, 1 - d_2$	1.7	25.1	37.0	30.2	3.8	3.1	0.8	52.0	48.0	73.0	27.0	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	Pyr	$1, 1 - d_2$	1.7	19.8	35.1	38.8	4.5	1.3	0.4	69.8	30.2	82.3	17.7	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	Pyr	$1, 1-d_2$	0.4	20.4	44.2	29.5	5.4	0.5	0.0	66.8	33.2	f	f	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	Pyr	$1, 1/3, 3-d_2^{o}$	0.4	26.9	54.0	10.3	8.9	0.0	0.0	31.6	68.4	f	f	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	Руг	1,1/3,3-d20.h	0.4	6.0	20.0	70.4	3.6	0.0	0.0	f	f	55.7	44.3	
Bi <sub>2</sub> O <sub>3</sub> · 3MoO <sub>3</sub>	_	$C_3^{=}-1, 1-d_2^{i}$	-	91.5	8.5	0.0	0.0	0.0	0.0	29.4	70.6		_	

<sup>a</sup> 0.25-sec contact time, 0.7 m<sup>2</sup> catalyst, AA + solvent = 32  $\mu$ mole total, unless otherwise stated.

 ${}^{b}C_{3}$  = propylene, AA = allyl alcohol, HD = 1,5-hexadiene, PhH = benzene, AE = diallyl ether.

<sup>c</sup> 2-MPyr = 2-methoxy pyridine, Pyr = pyridine.

<sup>d</sup> Ratios by NMR.

" Masked by pyridine peak.

<sup>1</sup> Not enough collected to analyze by NMR.

<sup>9</sup> 55:45 (1,1-d<sub>2</sub>:3,3-d<sub>2</sub>) mixture used.

<sup>h</sup> Contact time = 0.025 sec, 0.07 m<sup>2</sup> catalyst.

<sup>i</sup> Feed = 24.5  $\mu$ mole C<sub>3</sub><sup>2-</sup>-1,1-d<sub>2</sub>; 3.0 cm<sup>3</sup> (2.48 g, 4.2 m<sup>2</sup>) Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub>; 15-sec contact time.

fits well the theoretical maximum  $k_{\rm H}/k_{\rm D}$ [2.51 (320°C), 2.18 (430°C)]. However, for Bi<sub>2</sub>O<sub>3</sub> 3MoO<sub>3</sub> (Table 8), there is a net retention of original carbon integrity in the oxidation reaction, i.e., more acrolein-1-*d* is formed from allyl alcohol-1,1-*d*<sub>2</sub> and more acrolein -3,3-*d*<sub>2</sub> from the 3,3-*d*<sub>2</sub> isomer than expected, based on the isotope effect ( $k_{\rm H}/k_{\rm D} = 2.5$ ).

When the reaction of allyl alcohol-1,1- $d_2$ is run under conditions of low conversion  $(0.3-0.5 \text{ cm}^3 \text{ catalyst}, 0.25 \text{ sec})$  for both MoO<sub>3</sub> and Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub> incomplete isomerization to a mixture of allyl alcohol-1,1 $d_2$  and -3,3- $d_2$  occurs, the degree of which decreases in the following order: multicomponent  $\approx$ MoO<sub>3</sub> > Bi<sub>2</sub>O<sub>3</sub> · MoO<sub>3</sub>  $\approx$  Bi<sub>2</sub>O<sub>3</sub> · 3MoO<sub>3</sub>  $\gg$  Bi<sub>2</sub>O<sub>3</sub> (Table 4). The 1-d : 3,3- $d_2$ ratio of the acrolein isolated reflects an enrichment in the 3,3- $d_2$  component when compared to the allyl alcohol-3,3- $d_2$ : 1,1- $d_2$ ratio, due to the deuterium isotope effect.

(b) Reactions in the presence of base. In order to distinguish between acid-site and oxidizing-site isomerization, the effect of base on the isotopic distribution in the acrolein and unoxidized alcohol resulting from the reaction of allyl alcohol-1,1- $d_2$  at 320°C over MoO<sub>3</sub> and  $\alpha$ -bismuth molybdate was investigated. The results in Table 9 show that for these catalysts, less isomerization to allyl alcohol-3,3- $d_2$  and, correspondingly, less acrolein-3,3- $d_2$  formation occur when the reaction is run in the presence of sufficient base to eliminate acid sites. The fact that a substantial portion of the isomerization occurs in the presence of excess base indicates that both acid sites and acrolein-forming sites are responsible for interconversion of the two ends of the allylic species.

Several important features of these experiments run in the presence of base, which represent reaction on acrolein-forming sites only, are worthy of note. First of all, the ratio of acrolein- $3, 3-d_2$ : 1-d formed on both catalysts is much less than the 29:71 ratio observed for the reaction of propylene-1,  $1-d_2$  (Table 9) which results from a  $k_{\rm H}/k_{\rm D}$  isotope effect of 2.4, indicating that total equilibration of the isomeric allyl molybdates is not occurring. However, when compared to the  $3,3-d_2:1,1-d_2$  ratio in the isolated unoxidized alcohol, the acrolein-3,3- $d_2$ : 1-d ratio indicates that enough isomerization is occurring to result in an enrichment in the  $3,3-d_2$  component as expected based on a hydrogen-deuterium iso-



SCHEME 1. Reaction of propylene-1,  $1-d_2$  with molybdate catalysts.

tope effect of about 2.4. Furthermore, if one starts with a 1:1 mixture of allyl alcohol-1,1- $d_2$  and -3,3- $d_2$ , the same ratio of acrolein-3,3- $d_2$ : 1-d is obtained as that observed in the reaction of propylene-1,1- $d_2$ . These isotopic experiments show that there is not enough equilibration to accommodate a mechanism in which the  $\sigma$  O-allyl molybdate is formed directly from propylene, but sufficient equilibration does occur to be consistent with the initial formation of a  $\pi$ allyl intermediate, followed by formation of either  $\sigma$  O-allyl intermediate in equal amounts and subsequent H or D abstrac-



FIG. 4. <sup>16</sup>O Incorporation into acrolein and allyl alcohol from reaction of <sup>18</sup>O-allyl alcohol with MoO<sub>3</sub> at 320°C. 1.96 g (1.0 cm<sup>3</sup>, 1.4 m<sup>2</sup>) MoO<sub>3</sub>. Fresh catalyst used for each injection. Molar velocity = 83.5  $\mu$ mole sec<sup>-1</sup>.

tion to form acrolein-3,3- $d_2$  and -1-d in the expected ratio based on an isotope effect of 2.4 at 320°C (Scheme 1).

## Oxidation of <sup>18</sup>O-Allyl Alcohol over Mo<sup>16</sup>O<sub>3</sub>

The results in Fig. 4 show that a high degree of <sup>16</sup>O incorporation (low <sup>18</sup>O/<sup>16</sup>O) occurs in both isolated alcohol and acrolein at low pulse times (0.2 sec = 16.7  $\mu$ mole injected). This incorporation falls off with pulse time, faster for isolated alcohol than for acrolein, indicating that some <sup>16</sup>O incorporation must be associated with the path leading to acrolein on selective oxidation sites.

The amount of <sup>16</sup>O incorporation into acrolein is insensitive to base, while a basic reaction medium causes much less <sup>16</sup>O incorporation in the isolated alcohol (Table 10).

These results support a dual-site mechanism in which <sup>16</sup>O incorporation occurs on

TABLE 10

Effect of Base on <sup>18</sup>O-Allyl Alcohol Oxidation over MoO<sub>3</sub> at 320°C<sup>a</sup>

Diluent	18(	<sup>18</sup> O/ <sup>16</sup> O <sup>b</sup>				
	Acrolein	Allyl alcohol				
<i>n</i> -Octane	0.142	0.229				
Pyridine	0.123	0.670				

<sup>a</sup> 0.25 cm<sup>3</sup> (0.49 g) MoO<sub>3</sub> used; 0.06-sec contact time; alcohol; diluent ratio = 0.33, 3.5  $\mu$ l of 3.2 M in alcohol, 9.6 M diluent injected.

<sup>b</sup> Ratios by mass spectroscopy.

both acid and acrolein-forming sites, the latter process being insensitive to base.

## Ammoxidation-Nitrogen Incorporation Experiments

(a) Yield vs  $NH_3$ : allyl alcohol ratio, 380°C (Fig. 5). Experiments in which the ammonia: allyl alcohol ratio is varied from 0 to 9.2 show that six ammonia molecules



FIG. 5. Yields vs ammonia : allyl alcohol ratio for reaction with MoO<sub>3</sub> at 380°C. AA = allyl alcohol. 0.98 g (0.5 cm<sup>3</sup>, 0.7 m<sup>2</sup>) MoO<sub>3</sub> used. Fresh catalyst used for each run. Pulse size =  $1.9 \text{ cm}^3$  (35  $\mu$ mole total).



FIG. 6. Yields vs temperature in allyl amine oxidation over MoO<sub>3</sub>. 5.4 g (3 cm<sup>3</sup>, 3.8 m<sup>2</sup>) MoO<sub>3</sub>, 2 sec. Catalyst oxidized under air stream 30 min at 450°C between runs. 1  $\mu$ 1 of 2.9 *M* allyl amine in H<sub>2</sub>O injected at each temperature.

per allyl alcohol in the gas phase are required for maximum acrylonitrile (AN) formation to occur. No ammonia burning was observed in these experiments. Although the relative adsorption coefficients for allyl alcohol and  $NH_3$  are not known, these results suggest that there is a requirement for several ammonia molecules per allyl alcohol on the catalytic site for selective oxidation to achieve maximum AN yield.

(b) Reaction of allyl amine with  $MoO_3$ (Fig. 5). This reaction gave acrylonitrile as the major product, with substantial amounts of acrolein. At 320°C the carbon balance is very low (15%), but increases with increasing temperature. The inability of the active site to undergo the required four-electron reduction and the difficulty of desorption of acrylonitrile at the lower temperature are probably responsible for the low carbon balances. The presence of acrolein suggests that an initially formed Nbonded  $\sigma$ -complex can be converted to an O-bonded  $\sigma$ -complex, which is the acrolein precursor, although hydrolysis of an imine intermediate might also contribute to its formation.

### DISCUSSION

The reactions of allyl alcohol with MoO<sub>3</sub>,  $M_a^{2+}M_b^{3+}Bi_xMo_yO_z$ , and  $Bi_2O_3 \cdot nMoO_3$ (n = 0, 1, 3) can be divided into two main groups: alcohol isomerization and acrolein/propylene/diene formation. The proposed mechanisms for these processes are depicted in Schemes 2 and 3 for MoO<sub>3</sub>.

### Allyl Alcohol Isomerization (Scheme 2)

The isomerization reaction, namely, interconversion of allyl alcohol-1,1- $d_2$  and -3,3- $d_2$ , can be explained on the basis of two effects, namely, carbonium ion formation on acid/ether-forming sites and the interconversion of the isomeric allyl molybdate-1,1- $d_2$  and -3,3- $d_2$  (4), the acrolein precursors, on acrolein-forming sites. Interaction of allyl alcohol-1,1- $d_2$  with acid sites, represented in Scheme 2 as surface hydroxyls, results in dehydration to form a chemi-



SCHEME 2. Allyl alcohol-1,  $1-d_2/3$ ,  $3-d_2$  isomerization, ether formation, and oxidation over MoO<sub>3</sub>.

sorbed allyl cation, which can either react with another molecule of allyl alcohol to form ether, after loss of a proton, or give isomerized  $(3,3-d_2)$  allyl alcohol via 7-3,3 $d_2$  or starting alcohol  $(1,1-d_2)$  via 7-1,1- $d_2$ , or by direct hydration.

Interaction of allyl alcohol with an oxidizing site, represented as surface Mo=O double bonds, gives molybdate ester 4-1,1 $d_2$ , which can undergo rearrangement to 4- $3,3-d_2$  and subsequently desorb as allyl alcohol-3,3- $d_2$ . The importance of Mo=O double bonds in this process is depicted. Acrolein formation from each of these intermediates occurs with rate constants  $k_{\rm D}$ and  $k_{\rm H}$ , respectively. The equilibration here is not complete at 320°C, but can accommodate a faster C-H bond breaking to give the expected acrolein-3,3- $d_2$ : 1-d ratio (70:30), based on the reaction of propylene-1,1- $d_2$  (Table 9). The isomerization which occurs in the presence of base is due to interconversion of the  $\sigma$ -allyl molybdates 4-1,1- $d_2$  and 4-3,3- $d_2$ , either by a

Cope-type rearrangement (a formal 3,3sigmatropic shift) as shown in Scheme 2, or via C-0 cleavage to form an allyl/molybdate pair which then reforms the C-O bond on the other terminal carbon. By either path, the importance of the Mo=O is apparent and consistent with the higher degree of isomerization for MoO<sub>3</sub> than  $Bi_2O_3 \cdot 3MoO_3$  in the presence of base  $(27.8\% \text{ allyl alcohol}-3,3-d_2 \text{ for MoO}_3 \text{ vs})$ 17.7% allyl alcohol-3,3- $d_2$  for BiO<sub>3</sub> · 3MoO<sub>3</sub>, Table 9).

## Acrolein, Propylene, and Dimer Formation (Scheme 3)

The proposed mechanism for these reactions is shown in Scheme 3. Reaction of allyl alcohol with an oxidizing site produces 4, which upon 1,4-hydrogen transfer results in a two-electron reduction of Mo and production of acrolein.

Propylene formation occurs by the reaction of a reduced acid site with alcohol with dehydration to form 8 followed by dispro-



SCHEME 3. Acrolein, propylene, and dimer formation from allyl alcohol over MoO<sub>3</sub>.

portionation to regenerate an oxidized site. The 1,5-hexadiene results from further reaction of allyl alcohol with propylene precursor 8 and loss of water to form 9, which can disproportionate to give 1,5-hexadiene and the oxidized site.

Pyridine inhibits this propylene/dieneforming path by reacting with 8 and the reduced acid site. Inhibition of this path by water results because 8 and 9 are formed from dehydration reactions. The use of water or pyridine has little effect on the acrolein yield although both result in a large decrease in conversion due to a decrease in propylene and diene yields. Thus, only oxidizing and not acid sites are capable of forming the molybdate ester 4, the acrolein precursor.

The acrolein yield decreases, while the yield of diallyl ether and 1,5-hexadiene increases, upon increasing the initial concentration of allyl alcohol (Figs. 1 and 2). Propylene yield increases initially but then follows a downward trend in this series. The increase in diene yield is faster than that of ether at higher initial alcohol concentrations. This is in accord with the predictions of Schemes 2 and 3 in which the formation of acrolein requires the reaction of only one molecule of allyl alcohol, while that of diallyl ether or propylene requires two molecules and that of 1,5-hexadiene three.

The conversion to acrolein (and total conversion) is decreasing in the order  $Bi_2O_3 \cdot MoO_3 > Bi_2O_3 \cdot 3MoO_3 > MoO_3$ .

Thus, the presence of bismuth atoms at the acrolein-forming chemisorption site (Mo) enhances the rate of allylic hydrogen abstraction either by abstraction of hydrogen via Bi–O bonds or by providing a sink for the molybdenum to which it can transfer electrons after hydrogen abstraction by molybdenum oxygens. The fact that  $MoO_3$  has substantial activity toward oxidizing allyl alcohol to acrolein suggests the latter explanation. The multicomponent system is the most active in this series, due to an enhancement in its ability to be reduced resulting from favorable electronic and structural characteristics.

## Ammoxidation of Allyl Alcohol and Oxidation of Allyl Amine to AN (Scheme 4)

Several ammonia molecules per allyl alcohol are desired at the active site domain for maximum AN yield (see Results section). The incorporation of nitrogen to form acrylonitrile via a route analogous to that in Scheme 2 but with substitution of Mo=NH for Mo=O is consistent with the results and is shown in Scheme 4. Initial chemisorption of ammonia with MoO<sub>3</sub> serves to block allyl alcohol chemisorption on oxidizing sites and results in formation of 10. Reaction of 10 with allyl alcohol gives 11, which upon Cope rearrangement, similar to the  $4-1, 1-d_2/4-3, 3-d_2$  rearrangement (Scheme 2), gives  $\sigma$ -bonded N-allyl intermediate 12 as shown in Scheme 4. If only one ammonia molecule per alcohol site is



AMMOXIDATION OF ALLYL ALCOHOL:

SCHEME 4. Acrylonitrile formation from reaction of allyl alcohol or allyl amine with MoO<sub>3</sub>.

present, one of the NH groups in 11 would be replaced by O, and thus there would be a greater probability of forming acrolein. This is consistent with the oxidation of allyl amine, which initially produces  $\sigma$ -bond Nallyl species 13. This intermediate can form either N- or O-inserted products as shown in Scheme 4, since both nitrogen and oxygen are bonded to the molybdenum in 13. Hydrolysis of the imine formed from 13 could also contribute to acrolein formation.

## Mechanistic Interpretation in Terms of Selective Propylene Oxidation (Scheme 5)

The molybdenum(VI) esters 4, 5, and 6 [Eqs. (3)-(5)] generated from allyl alcohol are analogous to the proposed allylic intermediates 3 [Eq. (2)] and 14 (Scheme 5) in the selective oxidation of propylene (10, 11, 13). The results are interpreted in terms of the formation of this intermediate by initial chemisorption on Mo centers, followed by allylic abstraction by Bi oxygens giving  $\pi$ -allyl intermediate 15, which then collapses to form  $\sigma$ -complex 14, the acrolein precursor. The incorporation of nitrogen in ammoxidation to form acrylonitrile is analogous to that depicted in Scheme 4 and involves formation of a  $\sigma$ bonded N-allyl complex from an O-allyl species after catalyst N-incorporation via condensation of surface Mo=O double bonds with ammonia. Formation of AN results from two subsequent hydrogen abstraction reactions from this N-allyl complex as depicted in Scheme 5.

A comparison of this proposed selective oxidation mechanism with three other important mechanisms in the literature is shown in Table 11. There is a considerable amount of discrepancy here between the assignment of the role of the individual elemental components of the catalyst. Matsurma's results, based on low-temperature adsorption studies, attributes chemisorption and first hydrogen abstraction to Mo, while in Haber's mechanism, based on *in situ* generation of the allylic intermediate, the roles are reversed. Sleight, on the other hand, attributes all the steps shown here to  $MOQ_4^{2-}$  groups, while the bismuth



SCHEME 5. Mechanism for selective oxidation and ammoxidation of propylene over bismuth molybdate.

supplies an overlapping Bi/Mo conduction band (6p/4d), which serves as an electron sink. Our mechanism is based on a consideration of the reactions of both propylene and the allylic intermediate studied in this work by *in situ* generation from allyl alcohol. The former contains information concerning the initial chemisorption and the first  $\alpha$ -hydrogen abstraction, while the latter is important in understanding subsequent steps.

### CONCLUSIONS

In this work we have presented evidence that the reaction of allyl alcohol with  $MoO_3$ and  $Bi_2O_3 \cdot nMoO_3$  (n = 1, 3) occurs via

TABLE	1	1
-------	---	---

Step	Matsuura	Haber	Sleight	Grasselli et al.	
Olefin chemisorption	Mo (B site)	Bi	Мо	 Mo	
NH <sub>3</sub> chemisorption, NH formation	Mo (B site)	Мо	Мо	Мо	
1st allylic H abstraction	Mo (B site)	Bi	Мо	Bi	
2nd (3rd) H abstractions	Mo (B site)	Мо	Мо	Мо	
O(NH) insertion	Bi (A site)	Мо	Мо	Мо	
Electron flow	$e^- \rightarrow \mathrm{Bi} \rightarrow \mathrm{Mo} \rightarrow \mathrm{O}_2$	$e^- \rightarrow \mathrm{Mo} \rightarrow \mathrm{Bi} \rightarrow \mathrm{O}_2$	$e^- \rightarrow Mo \rightarrow Bi \rightarrow O_2$ (also Keulks)	$e^- \rightarrow Mo \rightarrow Bi \rightarrow O_2$	
Remarks	Site density (B) = $2 \times$ site density (A) A, high $\Delta$ H ads. B, low $\Delta$ H ads.	If no Mo present, $C_8H_{10}$ forms from 2 allyls.	$Bi_{6p}/Mo_{4d}$ overlap serves as $e^-$ sink.	Bi facilitates 2nd/3rd H abstractions by $e^-$ sink effect.	

Selective Oxidation Mechanism Comparisons

chemisorption on two types of sites: oxidation sites, on which acrolein is formed via allyl molybdates, and Brønsted acid sites, which form diallyl ether via allyl carbonium ion. Bismuth enhances the rate of  $\alpha$ -hydrogen abstractions, the rate-determining step in allyl alcohol oxidation to acrolein. The extent of the C-1/C-3 interconversion in the isomeric deuterium-labeled allyl molybdates generated from ally alcohol-1,1- $d_2$ and  $-3, 3-d_2$  is consistent with the formation of an analogous  $\sigma$  O-allyl molybdate (the acrolein precursor) via  $\pi$ -allyl molybdate in the selective oxidation of propylene. In ammoxidation, nitrogen incorporation occurs via a similar C-1/C-3 interconversion process on a surface in which surface Mo=O are replaced by Mo=NH. Thus, oxygen or nitrogen insertion prior to the second hydrogen abstraction is a likely mechanism in the selective oxidation and ammoxidation of propylene.

### ACKNOWLEDGMENTS

The authors acknowledge Dr. K. L. Gallaher and Dr. J. Shen of The Standard Oil Company (Ohio) for their assistance in NMR and mass spectroscopy analyses.

### REFERENCES

- Dadyburjor, D. B., Jewur, S. S., and Ruckenstein, E., Catal. Rev. 19, 293 (1979); Bielanski, A., and Haber, J., Catal. Rev. 19, 1 (1979); Gates, B. C., Katzer, J. R., and Schuit, G. C. A., "Chemistry of Catalytic Processes," pp. 325-389. McGraw-Hill, New York, 1979, Hucknall, D. J., "Selective Oxidation of Hydrocarbons," p. 24 ff and references therein. Academic Press, New York, 1977.
- Sachtler, W. M. H., and deBoer, N. H., in "Proceedings, 3rd International Congress on Catalysis, Amsterdam, 1964," p. 252. Wiley, New York, 1965; Adams, C. R., and Jennings, T., J. Catal. 2, 63 (1963); Adams, C. R., and Jennings, T., J. Catal. 3, 549 (1964); Adams, C. R., Voge, H. H., Morgan, C. Z., and Armstrong, W. E., J. Catal. 3, 379 (1964); Grasselli, R. K., and Suresh, D. D., J. Catal. 25, 273 (1972).
- 3. Keulks, G. W., and Krenzke, L. D., in "Proceedings, 6th International Congress on Catalysis,

London, 1976" (G. C. Bonds, P. B. Wells, and F. C. Tompkins, Eds.), p. 806. The Chemical Society, London, 1977. Keulks, G. W., J. Catal. 19, 232 (1970); Wragg, R. D., Ashmore, P. G., and Hockey, J. A., J. Catal. 22, 49 (1971); Hoefs, E. V., Monnier, J. R., and Keulks, G. W., J. Catal. 57, 331 (1979).

- Sancier, K. M., Wentreek, P. R., and Wise, H., J. Catal. 39, 141 (1975).
- Otsubo, T., Miura, H., Morikawa, Y., and Shirasaki, T., J. Catal. 36, 240 (1975); Miura, H., Otsubo, T., Shirasaki, T., and Morikawa, Y., J. Catal. 56, 84 (1979).
- Mars, P., and van Krevelen, D. W., Chem. Eng. Sci. Suppl. 3, 41 (1954); Dadyburjor, D. B., and Ruckenstein, E., J. Phys. Chem. 82, 1563 (1978).
- Giordano, N., Meazza, M., Castellan, A., Bart, J. C. J., and Ragaini, V., J. Catal. 50, 342 (1977); Sancier, K. M., Dozono, T., and Wise, H. J. Catal. 23, 270 (1971); Peacock, J. M., Sharp, M. J., Parker, A. J., Ashmore, P. G., and Hockey, J. A., J. Catal. 15, 379 (1969).
- Hart, P. J., and Friedli, H. R., J. Chem. Soc. D, 621 (1970).
- Orlov, A. N., and Gagarin, S. G., *Kinet. Catal.* 15, 1308 (1974); Callahan, J. L., Grasselli, R. K., Milberger, E. C., and Strecker, H. A., *Ind. Eng. Chem. Prod. Res. Develop.* 9, 134 (1970)
- Weiss, F., Marion, J., Metzger, J., and Cognion, J.-M. Kinet. Catal. 14, 32 (1973).
- Trifiro, F., Centola, P., Pasquon, I., and Jiru, P., in "Proceedings 4th International Congress on Catalysis, Moscow, 1968" (B. A. Kazansky, Ed.), p. 310. Adler, New York, 1968; Trifiro, F., and Pasquon, I., J. Catal. 12, 412 (1968).
- 12. (a) Davydov, A. A., Mikhaltchenko, V. G., Sokolovskii, V. D., and Boreskov, G. K., J. Catal. 55, 299 (1978); (b) Iwasawa, Y., Nakano, Y., and Ogasaware, S., Trans. Faraday Soc. I, 74, 2968 (1978).
- 13. Burrington, J. D., and Grasselli, R. K., J. Catal. 59, 79 (1979).
- I4. Grasselli, R. K., and Hardman, H. F., U.S. Patent 3,642,930 (Feb. 15, 1972); Grasselli, R. K., Miller, A. F., and Hardman, H. F., Ger. Offen. 2,147,480 (May 4, 1972); Grasselli, R. K., Miller, A. F., and Hardman, H. F., Ger. Offen. 2,203,709 (Aug. 17, 1972).
- McMichael, K. D., J. Amer. Chem. Soc. 89, 2943 (1967).
- Schuetz, R. D., and Millard, F. W., J. Org. Chem. 24, 297 (1959).
- Murty, A. N., and Curl, R. F., Jr., J. Chem. Phys. 46, 4176 (1967).
- Brazdil, J. F., Suresh, D. D., and Grasselli, R. K., J. Catal. in press.